

# Lecture 12: Viscous effects and phase separation kinetics

Linear non-equilibrium thermodynamics.

- Local thermodynamic equilibrium.
- Gradients in intensive variables, cause currents & fluxes of their conjugate variable.

Phenomenological laws:  $\vec{j}_i = \sum_k L_{ik} \nabla \phi_k$

Microscopic time reversibility:  $L_{ij} = L_{ji}$  (Onsager reciprocal relations)

*Annotations:*  
 -  $\vec{j}_i$ : current density  
 -  $L_{ik}$ : kinetic coefficients  
 -  $\nabla \phi_k$ : thermodynamic driving forces.

Entropy balance:  $\frac{\partial s}{\partial t} = -\nabla \cdot \vec{j}_s + \sigma$

*Annotations:*  
 -  $s$ : entropy density  
 -  $\vec{j}_s$ : entropy current density  
 -  $\sigma$ : entropy production.

$\sigma \geq 0$  (consequence of second law + imposing it locally)

Last lecture we only discussed energy and particle conservation

$$\frac{\partial \rho}{\partial t} + \nabla \cdot \vec{j}_\rho = 0 \quad \vec{j}_\rho = L_{\rho\rho} \nabla \left(-\frac{\mu}{T}\right) + L_{\rho\varepsilon} \nabla \left(\frac{1}{T}\right)$$

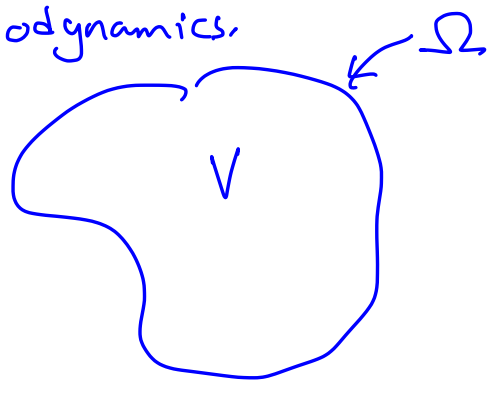
$$\frac{\partial \varepsilon}{\partial t} + \nabla \cdot \vec{j}_\varepsilon = 0 \quad \vec{j}_\varepsilon = L_{\varepsilon\rho} \nabla \left(-\frac{\mu}{T}\right) + L_{\varepsilon\varepsilon} \nabla \left(\frac{1}{T}\right)$$

We implicitly assumed the absence of viscous effects, or fluid flow.  
 In this lecture, we will include such effects consistent with 1<sup>st</sup> & 2<sup>nd</sup> law.

First, we will focus on the first law of thermodynamics.

Consider n-component mixture  
 $\rho_k$ : mass density of component k.

$$\frac{d}{dt} \int_V d\vec{r} \rho_k = \int_V \frac{\partial \rho_k}{\partial t} dV$$



$$\int_V d\vec{r} \frac{\partial \rho_k}{\partial t} = - \int_{\Omega} d\vec{S} \cdot (\rho_k \vec{v}_k) \stackrel{\text{Gauss}}{=} - \int_V d\vec{r} \nabla \cdot (\rho_k \vec{v}_k) \quad \text{valid for arbitrary } V.$$

material flow of component  $k$  into volume  $V$

$$\Rightarrow \frac{\partial \rho_k}{\partial t} = - \nabla \cdot (\rho_k \vec{v}_k)$$

$$\frac{\partial \rho}{\partial t} = - \nabla \cdot (\rho \vec{v})$$

$k=1, \dots, n.$  Sum all  $n$  equations:

$$\rho = \sum_{k=1}^n \rho_k \quad \text{total mass density. (in this lecture not a number density!)}$$

$$\vec{v} = \rho^{-1} \sum_{k=1}^n \rho_k \vec{v}_k \quad \text{barycentric or centre-of-mass velocity.}$$

conservation of mass

Can be augmented to include chemical reactions.

Alternatively, we can write:

$$\frac{D\rho_k}{Dt} = -\rho_k \nabla \cdot \vec{v} - \nabla \cdot \vec{J}_k \quad \vec{J}_k = \rho_k (\vec{v}_k - \vec{v}) \quad \text{"diffusion flow"}$$

$$\frac{D\rho}{Dt} = -\rho \nabla \cdot \vec{v}$$

$$\frac{D}{Dt} = \frac{\partial}{\partial t} + \vec{v} \cdot \nabla$$

material derivative or (barycentric) substantial time derivative.

Note that:  $\sum_{k=1}^n \vec{J}_k = 0$  Only  $n-1$  of  $n$  diffusion flows are independent.

Furthermore, we have balance of linear momentum:

$$\rho \frac{D\vec{v}}{Dt} = - \nabla \cdot \underline{P} + \sum_k \rho_k \vec{F}_k$$

body forces.

pressure tensor (minus the stress tensor)

Here, we assume that body forces are conservative:  $\vec{F}_k = -\nabla \psi_k$

and we define potential energy density  $\rho \psi := \sum_h \rho_h \psi_h$

Finally, we have the conservation of energy.

$$\frac{\partial \rho e}{\partial t} = -\nabla \cdot \vec{j}_e$$

Total specific energy:  $e = \frac{1}{2} \vec{v}^2 + \psi + u$

↑ kinetic energy of fluid     
 ↑ potential energy     
 ↗ specific internal energy.

We are interested in the part related to  $u$ .

Consider balance of linear momentum. Take inner product with  $\vec{v}$  and rewrite

$$\rho \frac{D}{Dt} \left( \frac{1}{2} \vec{v}^2 \right) = -\nabla \cdot (\underline{\underline{P}} \cdot \vec{v}) + \underline{\underline{P}} : \nabla \vec{v} + \sum_k \rho_k \vec{F}_k \cdot \vec{v}$$

$\underline{\underline{A}} : \underline{\underline{B}} = A_{\alpha\beta} B_{\beta\alpha}$      
 Since  $\rho \frac{Da}{Dt} = \frac{\partial(\rho a)}{\partial t} + \nabla \cdot (\rho a \vec{v})$

$$\frac{\partial}{\partial t} \left( \frac{1}{2} \rho \vec{v}^2 \right) = -\nabla \cdot \left( \frac{1}{2} \rho \vec{v}^2 \vec{v} + \underline{\underline{P}} \cdot \vec{v} \right) + \underline{\underline{P}} : \nabla \vec{v} + \sum_k \rho_k \vec{F}_k \cdot \vec{v} \quad (i).$$

Since  $\frac{\partial \psi_k}{\partial t} = 0$ , it follows from mass conservation that

$$\frac{\partial}{\partial t} (\rho \psi) = -\nabla \cdot \left( \rho \psi \vec{v} + \sum_k \psi_k \vec{j}_k \right) - \sum_k \rho_k \vec{F}_k \cdot \vec{v} - \sum_k \vec{j}_k \cdot \vec{F}_k \quad (ii).$$

This motivates us to decompose:

$$\vec{j}_e = \rho e \vec{v} + \underline{\underline{P}} \cdot \vec{v} + \sum_k \psi_k \vec{j}_k + \vec{j}_q \quad \text{which defines the heat flux.}$$

Insertion of  $\vec{j}_e$  in energy balance and using (i) & (ii):

$$\frac{\partial \rho u}{\partial t} = -\nabla \cdot (\rho u \vec{v} + \vec{j}_q) - \underline{\underline{P}} : \nabla \vec{v} + \sum_k \vec{j}_k \cdot \vec{F}_k.$$

internal energy not conserved!

We decompose:  $\underline{\underline{P}} = p \underline{\underline{I}} + \underline{\underline{\Pi}}$  ← viscous pressure tensor.  
↑ hydrostatic pressure

Then equation for specific internal energy  $u$  is:

$$\rho \frac{Du}{Dt} = -\nabla \cdot \underline{\underline{j}}_q - p \nabla \cdot \underline{\underline{v}} - \underline{\underline{\Pi}} : \nabla \underline{\underline{v}} + \sum_k \underline{\underline{j}}_k \cdot \underline{\underline{F}}_k$$

$$\rho \frac{Dq}{Dt} = -\nabla \cdot \underline{\underline{j}}_q$$

heat added per unit mass

$$\frac{Du}{Dt} = \frac{Dq}{Dt} - p \frac{Dv}{Dt} - v \underline{\underline{\Pi}} : \nabla \underline{\underline{v}} + v \sum_k \underline{\underline{j}}_k \cdot \underline{\underline{F}}_k$$

First law of thermodynamics with convection.

with  $v = \rho^{-1}$  the specific volume (volume per unit mass).

What about the second law?

Now  $s$  is specific entropy.

$$\frac{\partial \rho s}{\partial t} = -\nabla \cdot \underline{\underline{j}}_{s, \text{tot}} + \sigma \Leftrightarrow \rho \frac{Ds}{Dt} = -\nabla \cdot \underline{\underline{j}}_s + \sigma$$

$$\sigma \geq 0$$

$$\underline{\underline{j}}_s = \underline{\underline{j}}_{s, \text{tot}} - \rho s \underline{\underline{v}}$$

Local equilibrium:  $T ds = du + p dv - \sum_{k=1}^n \mu_k dc_k$

with  $c_k = \frac{\rho_k}{\rho}$  the mass fraction.

Local equilibrium:  $T \frac{Ds}{Dt} = \frac{Du}{Dt} + p \frac{Dv}{Dt} - \sum_{k=1}^n \mu_k \frac{Dc_k}{Dt}$

Furthermore  $\rho \frac{Dc_k}{Dt} = -\nabla \cdot \underline{\underline{j}}_k$

$$\vec{J}_s = \frac{1}{T} \left( \vec{J}_g - \sum_{k=1}^n \mu_k \vec{J}_k \right)$$

$$\sigma = \vec{J}_g \cdot \nabla \left( \frac{1}{T} \right) - \frac{1}{T} \sum_{k=1}^n \vec{J}_k \cdot \left( T \nabla \frac{\mu_k}{T} - \vec{F}_k \right) - \frac{1}{T} \underline{\underline{\Pi}} : \nabla \vec{v}$$

Heat flux is not uniquely defined, see de Groot & Mazur pp 25-27.

What about viscous pressure tensor.

We take  $\underline{\underline{\Pi}}$  s.t.  $\Pi_{\alpha\beta} = \Pi_{\beta\alpha}$  (no sources of torque)

We can always decompose  $\underline{\underline{\Pi}} = \frac{1}{3} \text{tr}(\underline{\underline{\Pi}}) \underline{\underline{1}} + \overset{\circ}{\underline{\underline{\Pi}}}$   
 $\uparrow$  traceless symmetric.

Similarly:  $\nabla \vec{v} = \frac{1}{3} (\nabla \cdot \vec{v}) \underline{\underline{1}} + \overset{\circ}{\nabla \vec{v}}$   
 $\uparrow$  traceless part.

then:  $\underline{\underline{\Pi}} : \nabla \vec{v} = \overset{\circ}{\underline{\underline{\Pi}}} : \overset{\circ}{\nabla \vec{v}} + \frac{1}{3} \text{tr}(\underline{\underline{\Pi}}) \nabla \cdot \vec{v}$   
 $\uparrow$  symmetric traceless  $\uparrow$   $\underline{\underline{\Pi}}$

Now we see that the entropy production splits as

$$\sigma = \underbrace{\vec{J}_g \cdot \nabla \left( \frac{1}{T} \right) - \frac{1}{T} \sum_{k=1}^n \vec{J}_k \cdot \left( T \nabla \frac{\mu_k}{T} - \vec{F}_k \right)}_{\text{vectorial}} - \underbrace{\frac{1}{T} \overset{\circ}{\underline{\underline{\Pi}}} : \overset{\circ}{\nabla \vec{v}}}_{\text{tensorial}} - \underbrace{\frac{1}{T} \Pi \nabla \cdot \vec{v}}_{\text{scalar}}$$

Thermodynamic fluxes do not depend on all components of thermodynamic forces  $\rightarrow$  Curie symmetry principle.

Can be proven (not here) that fluxes and thermodynamic forces of different tensorial character do not mix!

(6)

We conclude that:

$$\vec{j}_q = L_{qq} \nabla \left( \frac{1}{T} \right) - \sum_{k=1}^n L_{qk} \left( \nabla \frac{\mu_k}{T} - \frac{\vec{F}_k}{T} \right) \quad (\text{but no coupling with } \nabla \vec{v}!)$$

$$\vec{j}_i = L_{iq} \nabla \left( \frac{1}{T} \right) - \sum_{k=1}^n L_{ik} \left( \nabla \frac{\mu_k}{T} - \frac{\vec{F}_k}{T} \right)$$

$$\overset{\circ}{\Pi}_{\alpha\beta} = -\frac{L}{T} \left( \nabla \overset{\circ}{v}^s \right)_{\alpha\beta} = -\frac{L}{2T} \left( \partial_\alpha v_\beta + \partial_\beta v_\alpha - \frac{2}{3} \delta_{\alpha\beta} (\nabla \cdot \vec{v}) \right)$$

$$\Pi = -L (\nabla \cdot \vec{v}) / T.$$

Note all coefficients are scalars reflecting the underlying isotropic system! Generally they are tensors. Furthermore ORR:  $L_{iq} = L_{qi}$   
 $L_{ik} = L_{ki}$ .

Due to the Curie principle, we have moreover that scalar, vectorial, and tensorial parts of  $\sigma$  are separately positive definite.

It is insightful to focus on a one-component isotropic system: ( $\vec{F}_k = 0 \forall k$ )

$$\frac{\partial \rho}{\partial t} = -\nabla \cdot (\rho \vec{v}) \quad \text{Continuity equation.}$$

$$\rho \frac{D\vec{v}}{Dt} = -\nabla p + \eta_s \nabla^2 \vec{v} + \left( \frac{1}{3} \eta_s + \eta_b \right) \nabla (\nabla \cdot \vec{v}) \quad \text{Navier-Stokes}$$

$$\rho \frac{Du}{Dt} = \lambda \nabla^2 T - p \nabla \cdot \vec{v} + \underbrace{2\eta_s (\nabla \overset{\circ}{v})^s : (\nabla \overset{\circ}{v})^s + \eta_b (\nabla \cdot \vec{v})^2}_{\text{Rayleigh dissipation function}}$$

Here  $\eta_s = \frac{L}{2T}$  shear viscosity.

Equations of thermohydrodynamics.

$\eta_b = \frac{L}{T}$  bulk viscosity.  $\nabla \cdot$  No diffusion!

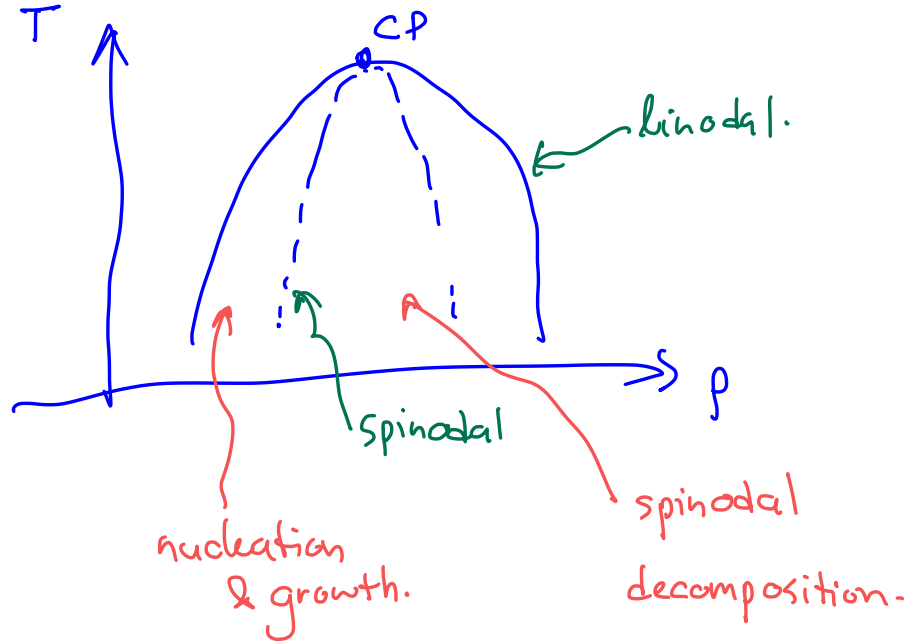
$\lambda = \frac{L_{qq}}{T^2}$  heat conductivity.

Above should be supplemented by  $p = p(\rho, T)$  and  $u = u(\rho, T)$ .

# Spinodal decomposition

Recall typical phase diagram of a system that can undergo

condensation:



To describe spinodal decomposition, we take purely diffusive isothermal dynamics:

$$\frac{\partial \rho}{\partial t} = D \nabla \cdot [\rho \nabla \beta \mu]$$

↳ let's interpret this as the intrinsic chemical potential.

$$= D \nabla \cdot \left[ \rho \nabla \frac{\delta \beta \mathcal{F}}{\delta \rho(\vec{r})} \right] \quad \text{Dynamical density functional theory}$$

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Lets take a square-gradient approximation:

$$F[\rho] = \int d\vec{r} \left[ f(\rho(\vec{r})) + \kappa |\nabla \rho(\vec{r})|^2 \right] \quad \kappa \text{ constant.}$$

$$\beta \mu(\vec{r}, t) = \frac{\partial f(\rho(\vec{r}, t))}{\partial \rho(\vec{r}, t)} - 2\kappa \nabla^2 \rho(\vec{r}, t).$$

$$\Rightarrow \frac{\partial \rho}{\partial t} = D \nabla \cdot \left[ \rho(\vec{r}, t) \frac{\partial^2 f(\rho(\vec{r}, t))}{\partial \rho(\vec{r}, t)^2} \nabla \rho(\vec{r}, t) - 2\kappa \rho(\vec{r}, t) \nabla (\nabla^2 \rho(\vec{r}, t)) \right]$$

Cahn-Hilliard equation.

Linearise:  $\rho(\vec{r}, t) = \rho_0 + \delta \rho(\vec{r}, t)$   $|\delta \rho(\vec{r}, t)| \ll \rho_0$

$\rho_0$   
constant  
bulk density.

$$\frac{\partial}{\partial t} \delta \rho(\vec{r}, t) = D \left[ \rho_0 \frac{\partial^2 f(\rho_0)}{\partial \rho_0^2} \nabla^2 \delta \rho(\vec{r}, t) - 2\kappa \rho_0(\vec{r}, t) \nabla^4 \delta \rho(\vec{r}, t) \right]$$

We solve in Fourier space:  $\delta \tilde{\rho}(\vec{k}, t) = \int d\vec{r} e^{-i\vec{k} \cdot \vec{r}} \delta \rho(\vec{r}, t)$

$$\Rightarrow \frac{\partial}{\partial t} \delta \tilde{\rho}(\vec{k}, t) = -D k^2 \left[ \rho_0 f''(\rho_0) + 2\kappa \rho_0 k^2 \right] \delta \tilde{\rho}(\vec{k}, t)$$

Solution:  $\frac{\delta \tilde{\rho}(\vec{k}, t)}{\delta \tilde{\rho}(\vec{k}, 0)} = \exp [R(k)t]$

$$R(k) = -D \rho_0 f''(\rho_0) \left[ 1 + \frac{2\kappa k^2}{f''(\rho_0)} \right] k^2$$

$\underbrace{\quad}_{\text{:= } D_{\text{coop.}}}$

"cooperative diffusion constant"

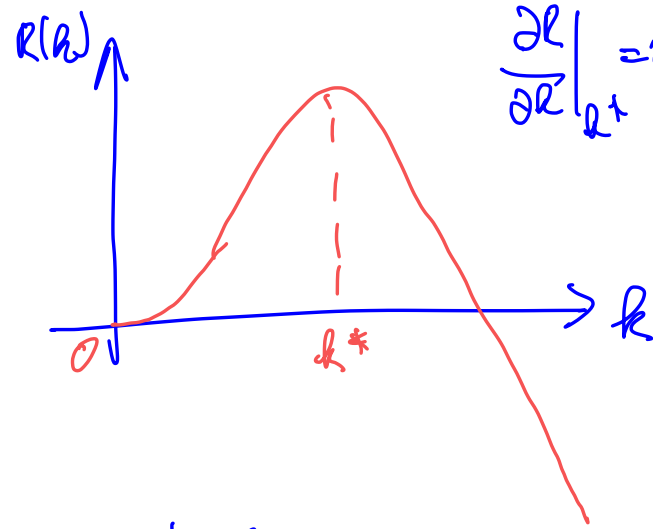
Note within spinodal  $D_{\text{coop}} < 0$  ("uphill diffusion")



Within spinodal: fluctuations amplify ( $R > 0$  for some  $k$ ).

Outside spinodal  $R < 0$  fluctuations relax.

Growth rate  $R(k)$



$$\frac{\partial R}{\partial k} \Big|_{k^*} = 0 \Rightarrow k_* = \left( \frac{-f''(p_0)}{4\kappa} \right)^{1/2} \sim \xi^{-1}$$

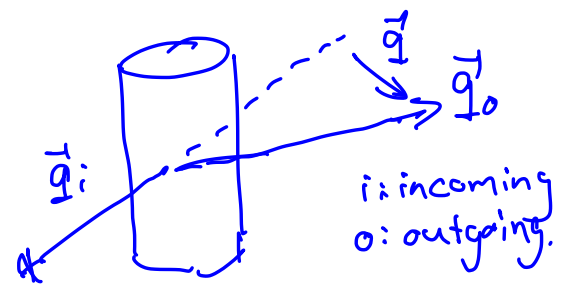
Deeper the quench  $\Rightarrow k_* \uparrow$

Typical length scale:  $k_*^{-1}$  (domain size)

$\Rightarrow$  finer the structure

Quench in unstable region produces instabilities that grow exponentially with time with one characteristic length scale that grows more quickly than others

Experimental determination via scattering

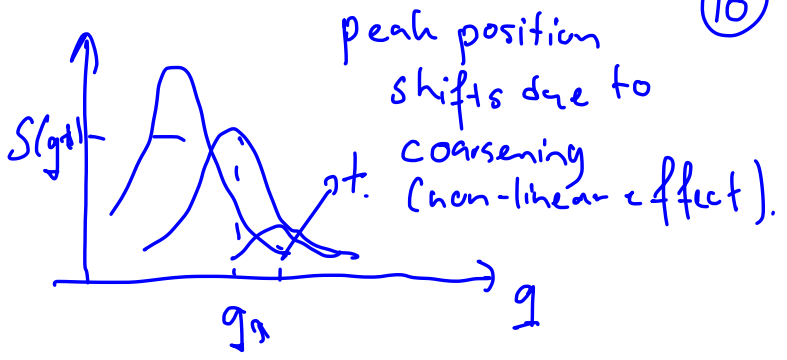
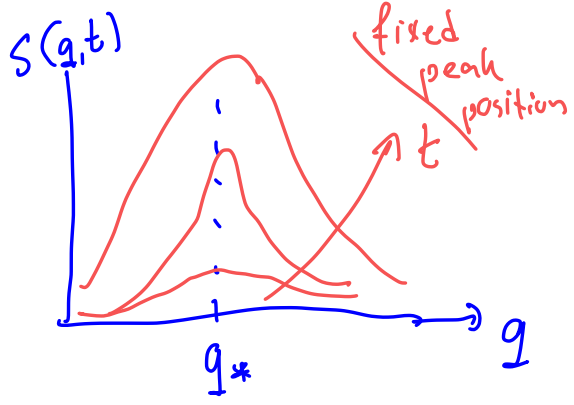


scattered intensity:  
 $I(\vec{q}, t) \propto S(\vec{q}, t)$   
 "dynamical structure factor"

$$S(\vec{q}, t) = \langle \delta \tilde{\rho}(\vec{q}, t) \delta \tilde{\rho}(-\vec{q}, 0) \rangle$$

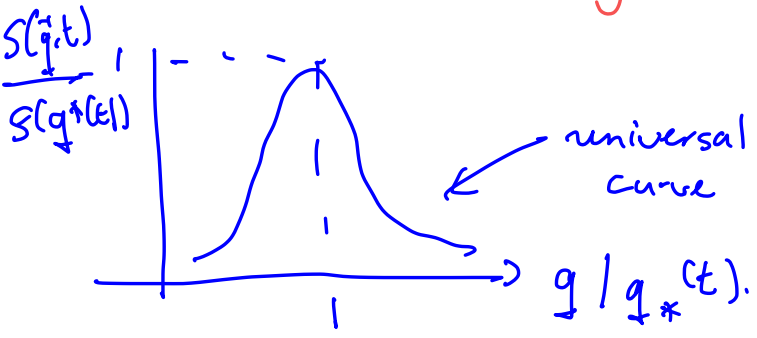
One can show that (Onsager regression hypothesis)

$$S(\vec{q}, t) = S(\vec{q}, 0) e^{R(\vec{q})t}$$



Linear Gahn-Hillard theory

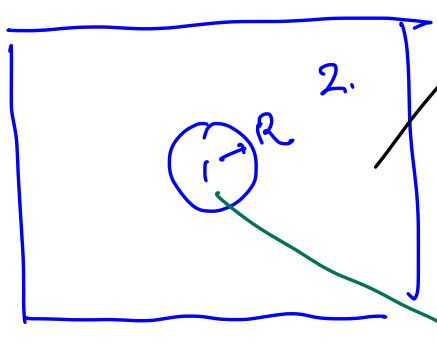
Experiment. Domain size grows!



Dynamical scale invariance.

(Slides!)

Nucleation and growth.



supercooled / supersaturated mixture.

droplet (nucleus) of new phase:

$$V = \frac{4}{3} \pi R^3$$

$$A = 4 \pi R^2$$

- Mixed state locally stable, but globally unstable. Locally stable  $\nRightarrow$  linearly stable.
- Relaxation to equilibrium requires non-linear  $\equiv$  large spontaneous fluctuation or external perturbation.
- Rate of formation can be estimated from thermodynamic arguments

Work done to create drop:  $\Delta G = N_A \Delta \mu + \gamma A$

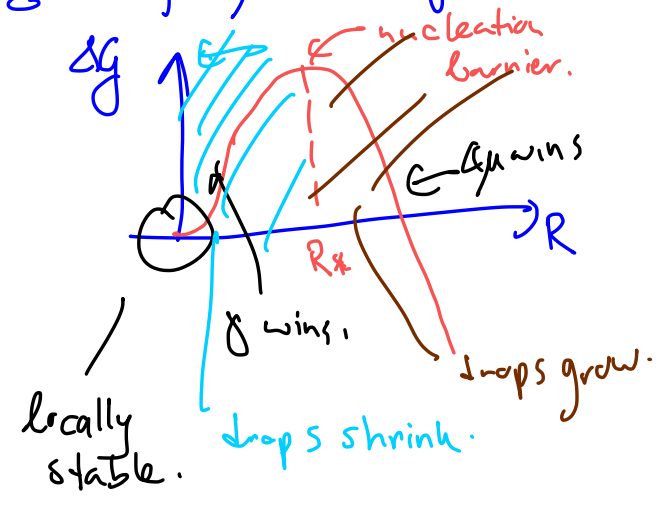
$\uparrow$   
# of A particles in drop.

Note that:   
 • Free energy gain  $\Delta\mu < 0$    
 •  $\gamma > 0$  free energy loss.  $\int \Rightarrow$  competition.

$\gamma, \Delta\mu$  computable from model free energy!

$$\Rightarrow \Delta G = \frac{4}{3}\pi R^3 \left( \frac{N_1}{\frac{4}{3}\pi R^3} \right) \Delta\mu + 4\pi R^2 \gamma = \frac{4}{3}\pi R^3 \rho_1 \Delta\mu + 4\pi R^2 \gamma.$$

$\rho_1$  density of A in drop, set by thermodynamics



Critical nucleus:  $\frac{\partial \Delta G}{\partial R} \Big|_{R_*} = 0$

$\Rightarrow R_* = 0$  (local minimum)

$$R_* = - \frac{2\gamma}{\rho_1 \Delta\mu} \text{ (maximum).}$$

Hence:  $N_* = \frac{32}{3}\pi \frac{\gamma^3}{\rho_1^2 |\Delta\mu|^3}$  (size critical nucleus)

$$\Delta G_* = \frac{16\pi\gamma^3}{3\rho_1^2 \Delta\mu^2}$$
 (nucleation barrier).

Note: (i) Near binodal:  $\Delta\mu \rightarrow 0 \Rightarrow N_* \rightarrow \infty \sim \Delta G_* \rightarrow \infty$

(ii) Near spinodal:  $\gamma \rightarrow 0 \Rightarrow N_* \rightarrow 0$

Steady-state nucleation rate.

$$j = K \rho_0 e^{-\beta \Delta G^*}$$

#nuclei per unit volume per second.

attempt frequency.

initial concentration.

Boltzmann factor accounting for probability that a critical nucleus is formed.

$\beta \Delta G^* \uparrow \Rightarrow$  slower nucleation.

